

THE LIQUID HYDROGEN SYSTEM FOR THE MUCOOL TEST AREA

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ABSTRACT

A new MuCool test area (MTA) is under construction at Fermi National Accelerator Laboratory. This facility will house a cryo-system composed of a liquid hydrogen absorber enclosed in a 5 Tesla magnet. The total volume of liquid hydrogen in the system is 25 liters. Helium gas at 14 K is provided by an in-house refrigerator and will sub-cool the hydrogen system to 17 K. Liquid hydrogen temperature in the absorber is chosen to satisfy the requirement of a density change smaller than $\pm 2.5\%$. To accommodate this goal and to remove the heat deposited by a beam, a pump will circulate liquid hydrogen at a rate of 450 g/s. The cooling loop was optimized with respect to the heat transport in liquid hydrogen and the pressure drop across the pump. Specific instrumentation will permit an intrinsically safe monitoring and control of the cryo-system. Safety issues are the main driver of the cryo-design.

This paper describes the implementation of the liquid hydrogen system at MTA and the preliminary results of a finite element analysis used to size the LH₂ absorber force-flow.

INTRODUCTION

In the framework of Muon Collider and Neutrino Factory research [1], a Mucool Test Area (MTA) cryo-system is being developed at Fermilab to run components of a cooling cell together under a high power beam test. This experiment will test the feasibility of ionization cooling for an intense ionizing beam passing through a LH₂ energy absorber.

Ionization cooling implies that the beam is “cooled” by energy loss and its emittance is reduced; both transverse and longitudinal momentum is lost to collisions with atomic electrons. The beam transversal momentum is damped by ionization energy loss in an energy-absorbing medium like LH₂ and the longitudinal momentum is restored by the RF acceleration between the LH₂ absorbers [2]. Energy loss and Coulomb scattering are in competition in the process of emittance reduction. To maximize the emittance reduction, the smallest atomic number is requested. Because of its small atomic number, LH₂ is the best candidate for ionization cooling. Since LH₂ needs to be contained and since any material in between the LH₂ medium and vacuum provokes undesirable Coulomb scattering effects, a material with a long radiation length is requested. Since beryllium has a questionable safety record, then aluminum becomes the optimal material to contain LH₂.

On the basis of the previous requirements, several LH₂ absorbers have been designed . Two potential heat transfer conditions are retained to remove the beam energy deposited in LH₂, while limiting the LH₂ density fluctuations to +/- 2.5 % and preventing LH₂ to reach its boiling point. Heat transfer by force-flow or by convection would satisfy the physical requirements. For both LH₂ absorber types, cold helium is used to maintain LH₂ properties. Although the very first LH₂ test to take place at MTA will consist in the KEK convection type LH₂ absorber, the subject of the current paper focuses on the implementation of the more demanding force-flow cryogenic system. Simulations of the force-flow behavior in the LH₂ absorber with respect to the cryogenic system capacities are introduced in the last section of this paper.

A realistic section to be tested at the MTA is composed of an intense ionizing beam passing through a LH₂ absorber, which is in series with RF cavities and embedded in a magnetic field [1]. The first stage of the cooling-channel components test at MTA will focus on the cryogenic feasibility of LH₂ absorber cooling. Therefore the first test with a LH₂ absorber will not use an intense ionization beam but, instead, electrical heaters will rather simulate energy deposition in the force-flow LH₂ absorber.

Hydrogen, nitrogen and helium are the cryogens of interest for the force-flow LH₂ absorber cryo-system. Parameters of the LH₂ cryo-system are summarized in table 1.

TABLE 1. MTA Cryo-system General Operating Parameters

Item	Value	Unit
Volume of the LH ₂ loop	25	liter
Volume of the vacuum space	35,000	liter
Refrigeration capacity	500	W
Refrigeration max mass flow	27	g/s
Refrigeration operating temperature	14	K
Refrigeration operating pressure	0.2	MPa
LH ₂ heat removal capacity	500	W
LH ₂ operating temperature	17	K
LH ₂ operating pressure	0.12	MPa
LH ₂ density	74.28	kg/m ³
H ₂ boiling point 0.12 (0.21 MPa)	21 (24)	K
H ₂ freezing point at 0.12 (0.21 MPa)	14	K
LH ₂ viscosity	3.05	10 ⁻⁶ Pa-s
LH ₂ specific heat	7696	J/Kg-K
Heat of vaporization	445.6	KJ/Kg
LH ₂ thermal conductivity	97	mW/m-K
20 degree C: liquid H ₂ volume ratio	790	-

CRYOGENIC FACILITIES

Cryogenic at MuCool Test Area

MTA cryo-system may be logically divided up into the hydrogen cryo-system and one onsite helium refrigeration system. Figure 1 shows the MTA buildings in beneficial occupancy planned for October 2003. MTA is mainly composed of the experimental hall, refrigerator room, compressor room, hydrogen manifold room and service building. The MTA experimental hall is an extension of a new beam line originating from the existing Fermilab 400 MeV proton Linac.

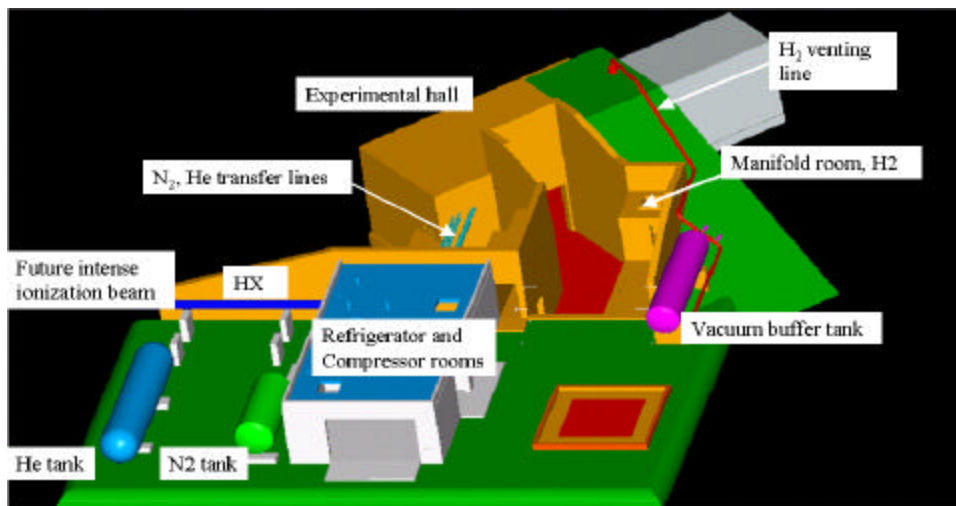


FIGURE 1. MuCool Test Area Buildings 3-D view

The MTA experimental hall will house the LH_2 absorber cryostat, a superconducting solenoid magnet, superconducting RF cavities, a magnet string and the intense ionizing beam line passing through the experimental hall. The so-called Lab G superconducting solenoid magnet is cooled by LHe and utilizes a LN_2 thermal shield. The superconducting solenoid design magnetic field is 5 Tesla.

The compressor room will house two 400 HP 2-stage oil injected screw compressors, which supply high-pressure helium gas to the refrigerator room.

Gas helium is supplied by a 34,000 liters helium storage tank located outside the refrigerator room. A complete satellite refrigeration system supplies 14 K helium gas to exchange heat and maintain the 25 liters of LH_2 at nominal conditions. Refrigerator heat exchanger shell side cooling is supplied by a dual cylinder 30 K reciprocating expansion engine. Cold high-pressure helium gas is then expanded through a reciprocating engine to achieve 14 K, 0.22 MPa helium gas to supply the MTA He/ LH_2 heat exchanger via a liquid nitrogen shielded transfer line. The nominal 14 K helium mass flow is 30 g/s.

The helium supply is used to cool the hydrogen from room temperature down to a liquefying temperature below 20 K. During nominal conditions, LH_2 is sub-cooled to 17 K, 0.12 MPa and circulates in a closed loop inside the MTA LH_2 absorber cryostat. MTA helium refrigeration system can provide up to 500 W of cooling capacity at 14 K to be distributed between the beam load and the system intrinsic loads.

Gaseous hydrogen is distributed from the manifold room to the experimental hall. Three hydrogen gas cylinders are stored in the manifold room but only one bottle will be open at a time for safety reason. Figure 2 shows the process and instrumentation diagram of MTA cryo-system and gives an idea of the different flows and parts interconnections.

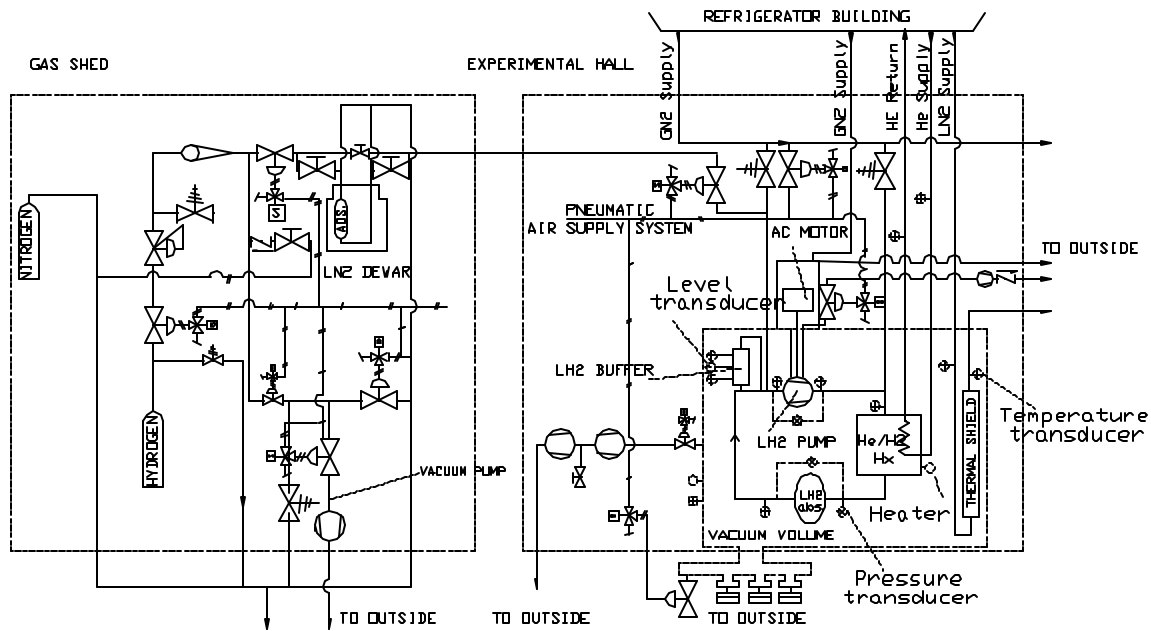


FIGURE 2. Simplified process and Instrumentation Diagram of MTA cryo-system

LH₂ Absorber Cryostat

The function of the MTA LH₂ absorber cryostat is to contain the LH₂ loop and to provide the interface with the rest of the cryo-system including the helium, nitrogen and hydrogen transfer lines. MTA LH₂ absorber cryostat vacuum vessel is mainly composed of a 0.41 m diameter pipe inserted inside the 0.44 m magnet bore and a 1.27 m diameter pipe located outside of the magnet bore. The maximum allowable working pressure (MAWP) of the MTA LH₂ absorber cryostat vacuum vessel is 0.17 MPa. The insulation vacuum is of the order of 1.3×10^{-4} Pa and the external pressure is the atmosphere. Figure 3 shows the 3D solid model of the MTA LH₂ absorber cryostat.

Thin aluminum windows close the MTA LH₂ absorber cryostat. As for the LH₂ absorber window, the beam passing through the windows shall interact with a minimum of matter. The shape of these aluminum vacuum windows is similar to the aluminum LH₂ absorber windows.

The MTA LH₂ absorber cryostat thermal shield consists of 4 mm thick aluminum semi-circular shields closed at its edges by G10 supports to reduce forces applied in case of quench of Mucool superconducting solenoid. Flat sheets protect the non-cylindrical sections of the MTA vacuum vessel. A wrap of 30 layers of MLI surrounds the thermal shield. The MTA cryostat thermal shield is cooled by LN₂ flowing in aluminum ½-inch IPS cooling pipes.

The supporting systems are composed of G10 material spiders supporting the cryostat vacuum vessel, thermal shield, LH₂ absorber and LH₂ pump and piping. G10 material is chosen to limit heat loads from the ambient to the LH₂ loop and to withstand the forces generated during cool down, nominal and quench conditions.

The total volume of the insulation vacuum in which the MTA LH₂ absorber is contained must be 790 times larger than the hydrogen cryo-loop capacity in order to withstand the saturated LH₂ expansion if a rupture of the system should occur. Therefore a 22.4 m³ vacuum buffer tank is connected to the MTA LH₂ absorber cryostat vacuum vessel via a 0.2 m venting pipe to be in accordance with the safety requirements.

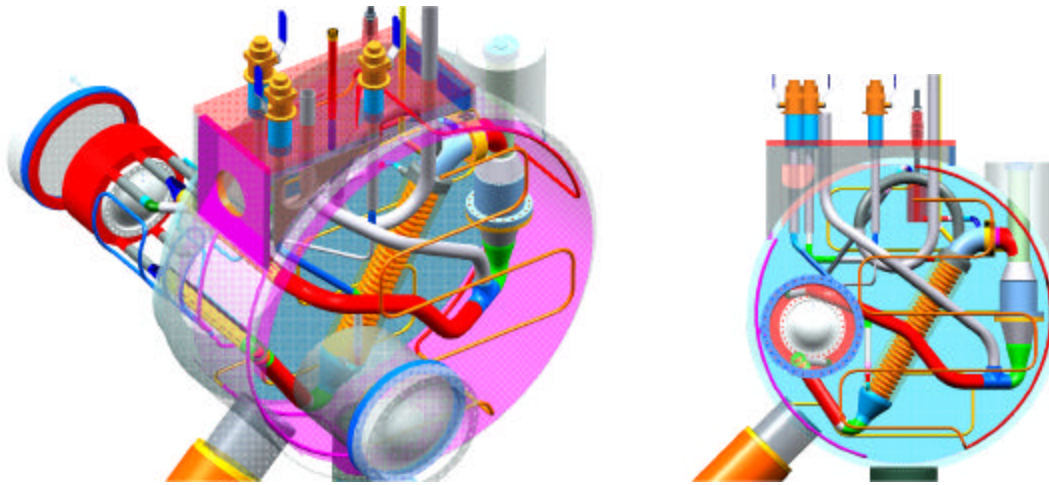


FIGURE 3. 3D Solid Model of MTA Cryostat

Safety Issues

Safety is the primary concern in designing the MTA cryo-system. The use of hydrogen imposes to follow strident design, fabrication, installation and operation requirements. The 25 liters in the LH₂ loop have an explosive yield equivalent to about 43 kg of TNT. Careful design and handling of hydrogen safely during the MTA cryo-system operations is a must. The cryo-design provides a safe vent path in the events of a failure in the LH₂ loop or accidental boil-off of hydrogen and is in accordance with ASME, NEC and Fermilab requirements.

Redundant safety features are designed to prevent a hazardous condition when a component fails. Barriers or safeguards are provided to minimize risks and control failures. A safety PLC for process controls and interlock mechanisms named QUADlog® is used. In the case of an emergency, the QUADlog® safety PLC will turn off all vacuum pumps close appropriate automatic valves and allow the system to vent to equilibrium. Control valves and control heaters permit to stabilize the cryo-system and especially the LH₂ flow. Interlocks to process instrumentation are being established. All electrical devices inside or at the vicinity of MTA LH₂ absorber cryostat must be rated Class I, Division II, group B, or being installed in an intrinsically safe configuration in agreement with NEC safety requirements. Elements of design like the use of capacitance manometers, low excitation current, excess flow valve, continuous N₂ purging venting lines shall prevent the mixture of hydrogen gas with the oxygen in air in the presence of an ignition source that could lead to an explosion. The equipment, power, and other system services shall be verified for safe performance in the design and normal operational regimes through certification. As mentioned previously a large vacuum buffer tank is connected to the MTA LH₂ absorber cryostat in order to contain all hydrogen gas that would expand to the standard pressure and temperature. Oxygen Deficiency Hazard (ODH) was also considered to design and instrument MTA buildings and ODH detectors are installed in MTA enclosure. 2,000 SCFM exhaust fans are mounted in the MTA experimental hall and manifold room. No recovery of H₂ is planned. For safety reasons, the venting lines outside of the experimental hall will relieve gaseous hydrogen in an area protected by a fence.

In order to anticipate for future run including an intense ionization beam, radiation can become an issue and materials radiation hardness are preferred.

Operating procedures for normal and emergency conditions were established and a special safety committee was appointed to review all characteristics of the cryo-system.

LH₂ FORCE-FLOW

LH₂ circuit

Gaseous hydrogen is liquefied during cool-down by heat exchange with the cold helium, which is supplied from the refrigerator room at 14 K and heated to 17 K before entering the LH₂ absorber cryostat. The LH₂ circuit volume is filled with gaseous hydrogen, which is slowly liquefied by helium refrigeration while maintaining a constant pressure. The process of filling is slow enough so that the energy generated by transformation from ortho-hydrogen to para-hydrogen is negligible. When the 25 liters of LH₂ are at nominal conditions in the LH₂ absorber, the flow is isolated and the LH₂ pump generates a force-flow able to remove the energy deposited by the beam in the LH₂ absorber. During nominal operation, LH₂ cryo-system contains 25 liters of LH₂ at 17 K and 0.12 MPa.

Instrumentation is imbedded in the LH₂ absorber and LH₂ circuit to determine temperature profiles, pressure distribution and to measure the flow of LH₂. Operating temperatures and pressure shall permit to stay below LH₂ boiling point. The LH₂ force-flow design is based on the capacity to remove energy from the LH₂ absorber while keeping a LH₂ density change less than 5 % and by limiting the loop pressure drop to the capacity of the available LH₂ pump. LH₂ circulates in a closed loop to remove the energy deposited in the LH₂ absorber volume through a counter flow LH₂/He heat exchanger [3]. The 17 K heat load budget distribution for the MTA force-flow LH₂ absorber test is estimated to 150 W (extended to 300 W) from the equivalent of the intense ionizing beam passing through a LH₂ absorber, 50 W from the LH₂ pump and 50 W from the ambient to the LH₂ loop. Taking into account additional engineering margin, the heat exchanger is sized for a cooling capacity of 500 W at 17 K. Based on this condition the proposed heat exchanger is a coil made of copper tube. Helium flows inside the copper pipe and LH₂ flow around the tubing. 27 turns form a coil of 89 mm diameter, which is housed in the heat exchanger outer shell. The 7.6 m long copper tube inner diameter is 15.8 mm its wall thickness is 0.8 mm. The heat transfer surface is about 0.34 m².

The piping system connecting the LH₂ absorber, LH₂ pump and LH₂/He heat exchanger is composed of stainless steel 25 mm and 50 mm pipe lines. Bimetallic junctions, which are certified to helium leak test on the order of 1×10^{-8} , are used between aluminum LH₂ absorber and stainless steel piping system. All pipes are welded to limit the risk of hydrogen leaking to the insulation vacuum. The 6.9 liter LH₂ absorber is composed of two thin aluminum windows and one aluminum manifold. Double indium seals are used to seal the two thin windows to the manifold. Holes in the manifold direct LH₂ flow towards the center of the LH₂ window, providing turbulence in the absorber volume to limit the density change.

For the current design the temperature rise was kept within 4 K. The admissible pressure drop through the LH₂ absorber represents about 50% of the total admissible pressure drop in the LH₂ circuit. The total admissible pressure drop in the LH₂ circuit is determined by the LH₂ pump characteristics and the pressure drop across it [4]. For instance, the total admissible pressure drop in the LH₂ circuit shall be less than 2,500 Pa if the LH₂ pump circulates 450 g/s of flow in the LH₂ circuit.

Heat Transfer Numerical Calculations

The design of the LH₂ absorber manifold requests a specific attention. It is important that the thermal power due to the beam is removed quickly and efficiently to reduce the risk of hydrogen boiling and thermal stresses in the thin aluminium windows. The

temperature must be uniform in the LH₂ absorber to prevent hot spot and LH₂ boiling. The pressure drop of the hydrogen must be kept low enough to meet the pressure drop limits of the LH₂ pump. The main concerns are the LH₂ flow temperature and pressure difference through the LH₂ absorber manifold. The LH₂ absorber manifold hole distribution is of critical importance. For this reason, Computational Fluid Dynamics (CFD) was carried on to establish the effect of hole orientations and sizes that can achieve the thermal performance targets and still comply with the given design constraints. The CFD software used for this study is the CFX, which is now part of ANSYS. The current analysis does not include the metallic window.

The CFD model inputs are the beam energy deposition, LH₂ properties, the absorber geometry and the velocity of LH₂ at the inlet of the holes. Figure 4a, 4d and 4e show the geometry of the 3-D model studied. The 3σ gaussian distribution beam energy was modeled as a continuous heat source with a uniform spread diameter of 10 mm passing through the LH₂ volume as observable in Figure 4d. The velocity is deduced from the available hydrogen loop mass flow rate and the hole diameter.

Two models were set up, one without the main inlet chamber as shown in Figure 4a and 4d and the other with an inlet chamber. In the model without the inlet chamber, flow is applied directly on each of the 15 inlet nozzles to the absorber, imposing a uniform flow rate on each of them. In the model with the inlet chamber, flow is applied to each of the two main inlets, which has a 25.8 mm bore. This latter case may not result in a uniform flow rate at each of the 15 inlet nozzles to the absorber. The ratio of the flow rate at the main inlet at the chamber to the individual inlets to the absorber is approximately 2.2 : 1.

Several nozzle distributions were studied for each model and in particular for the one with the velocity is applied to the chamber inlet. Configuration A represents 11 inlet and 15

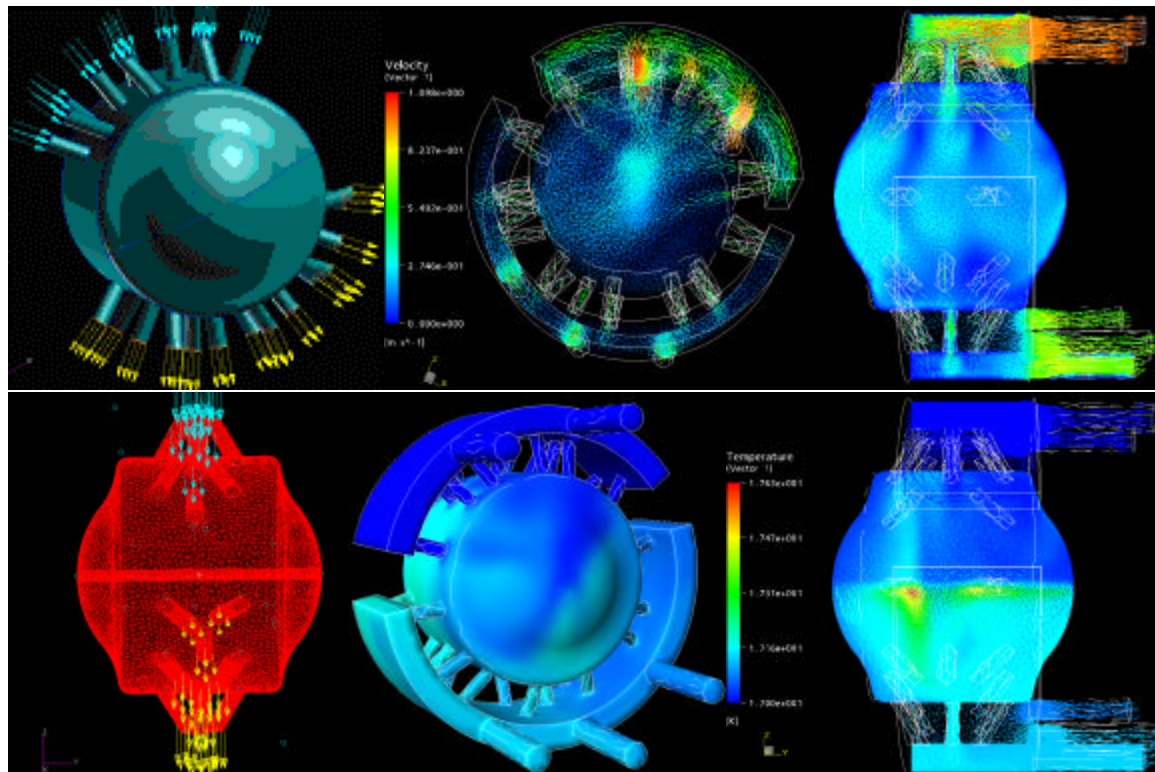


FIGURE 4. Configuration B with 300 W of beam power simulation, $v=4$ m/s; 4a) CFD model with flow direction; 4b) velocity distribution front view; 4c) velocity distribution side view; 4d) meshing with beam; 4e) temperature distribution and inner chamber visible; 4f) temperature distribution.

outlet nozzles, Configuration B represents 15 inlet and 19 outlet nozzles. The results of this analysis underlines that inlet nozzles distribution must be symmetric to allow smaller temperature rise hence the maximum energy removable. Figure 5 shows the influence of the velocity for these two symmetrical distribution configurations and shows that the use of more nozzles is not favorable to a temperature decrease but permit to limit pressure drop. Since the pressure drop in the system is the parameter of importance, configuration like 15 inlet and 19 outlet nozzles with a mass flow around 160 g/s is a good compromise.

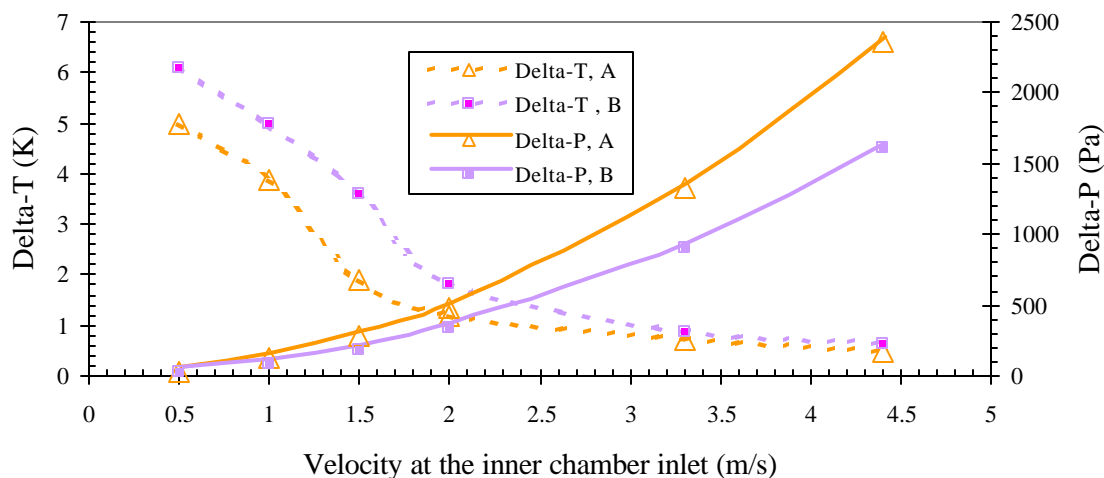


FIGURE 5. Influence of the velocity for configuration A and B. Delta-T is the maximum temperature difference obtained in the LH₂ absorber, Delta-P is the pressure drop between inner chamber inlet and outlet

CONCLUSION

This paper summarizes the development of the LH₂ system for the MuCool Test Area where the first components of the MuCool cooling channel, being LH₂ absorber will start to be tested in October 2003. The cryo-system is designed to be in compliance with safety codes. CFD results permit to address the LH₂ force flow design and permit to understand the interdependence between the LH₂ flow characteristics.

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